



Research Progress of Manganese-Based Catalysts in Low-Temperature Denitration

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Abstract

Low temperature denitration technology is a hotspot in recent years. Manganese-based catalysts are demonstrated to be most promising catalysts at low temperature. Many researchers have improved manganese-based catalysts from different aspects to meet the requirements of low-temperature catalysts. This paper attempts to review the progress of manganese-based catalysts from catalyst morphology, catalyst carriers, composite manganese-based catalysts and catalyst preparation methods in recent years, and the existing problems are also analyzed in the review.

Keywords: Low-temperature denitration; Manganese-based catalysts; NH_3 -SCR

Mini Review

Atmospheric contaminant treatment becomes an important research topic in recent years with the strict requirements of environmental protection. Nitrogen oxides (NO_x), which emitted from stationary sources (e.g., coal-fired power plants) and mobile sources (e.g., vehicle exhausts), is one of the major air pollutants. It can cause not only photochemical smog and acid rain, but also ozone depletion and greenhouse effect [1]. Many methods are used in applied and fundamental studies about denitration catalyst. Among them, The Selective Catalytic Reduction of NO_x by NH_3 (NH_3 -SCR) is to date the best developed and most widespread method for NO_x removal from stationary sources, and the general NH_3 -SCR reaction is: $4\text{NO} + 4\text{NH}_3 + \text{O}_2 = 4\text{N}_2 + 6\text{H}_2\text{O}$ [2]. Commercial technology, which employing V_2O_5 - WO_3 (or MoO_3)/ TiO_2 as catalyst [3], exhibits excellent catalytic performance in the temperature range of 300-400 °C. However, there are still some disadvantages as follows [4-7]: (1) V_2O_5 is easy to sublime in the using process, which causing biological toxicity when it enters into the environment; (2) SO_2 durability is unsatisfactory. The low temperature denitration technology (<200 °C) can place the SCR device in the low temperature and low dust section at the end of the flue gas treatment system, which can reduce the poisoning and mechanical wear of the catalyst. It is a meaningful work to develop low-temperature NH_3 -SCR catalysts, therefore, many efforts have been made to develop novel non-vanadium-based metal oxide

denitration catalysts with merits of high low-temperature efficiency and environment friendly.

Many investigations have been carried out on low-temperature NH_3 -SCR reaction. In comparison, manganese species have been demonstrated to be higher NO_x conversion at low temperatures. Pena et al. [8] studied the removal of NO by transition metal oxide/ TiO_2 under low temperature conditions and found that the denitration efficiency of different metal oxides is $\text{Mn} > \text{Cu} > \text{Cr} > \text{Co} > \text{Fe} > \text{V} > \text{Ni}$. It is believed that the transfer of electrons between different valence manganese species is very rapid, and it is conducive to improve NH_3 -SCR low-temperature activity. Huang et al. [9] prepared pure MnO_x (MnO , Mn_3O_4 , Mn_2O_3 , MnO_2) catalysts in NH_3 -SCR reaction, the results showed that MnO_2 is more suitable than other manganese oxides. Kapteijn et al. [10] studied the denitration performance of MnO_x with different valence states, and the conclusion is similar to Huang & Luo et al. [11] loaded MnO_2 with different crystal on TiO_2 -palygorskite (TiO_2 -Pal) and found that γ - MnO_2 gave higher activity than δ - MnO_2 and γ - MnO_2 . MnO_2 particles had a better dispersion in the carrier when mass ratio of Pal to TiO_2 was 2:1.

Ordinary manganese-based catalysts cannot meet the requirements of low temperature catalysis. In recent years, many researchers have improved manganese-based catalysts from different aspects to meet the requirements of low-temperature

catalysts. This paper attempts to summarize the progress of manganese-based catalysts from catalyst morphology, catalyst carriers, composite manganese-based catalysts and changing catalyst preparation methods in recent years.

Change catalyst morphology Tian et al. [12] prepared different morphologies MnO_2 using different methods. The results indicated that nanorods MnO_2 contributed the better denitration effect, and it was due to the large amount of strong acid sites, low crystallinity and more lattice oxygen. Hu et al. [13] prepared Mo(x)-MnOx rectangular nanorod catalyst by co-precipitation method. The corresponding catalytic performance and anti- H_2O performance increased significantly. Moreover, nanorod-formed catalysts have higher concentrations of Mn^{4+} , richer surface adsorption of oxygen (promoting NO oxidation to NO_2 and "fast-SCR" processes) and active sites. Also, the Mo(x)-MnOx nanorod catalyst has stronger acidity to adsorb ammonia species, which is also beneficial for increasing the catalytic activity of the catalyst. Li et al. [14] prepared MnFeOx nanorods used a hydrothermal method, and the results indicated that the $\text{MnFeO}_{1.0}\text{Ox}$ nanorods exhibited the highest NO conversion rate in NH_3 -SCR reaction. It was due to $\text{MnFeO}_{1.0}\text{Ox}$ nanorod catalysts obtained higher oxidation activity of NO to NO_2 . Li et al [15] prepared a three-dimensional flower-like NiMnFeOx mixed oxide catalyst and found that the structure of the three-dimensional flower-like NiMnFeOx mixed oxide can improve the NH_3 -SCR performance significantly. Li et al. [16] prepared a CeO_2 - MnOx catalyst with core-shell structure by chemical precipitation method, and the denitration rate reached over 90% at 110~220 °C.

Supported manganese-based catalysts YAO et al. [17] investigated the catalytic performance of manganese species on different supports and established a related reaction model. The results show that $\gamma\text{-Al}_2\text{O}_3$ can provide the highest dispersion, most acidic sites and excellent NOx absorption capacity. Huang et al. [18] loaded Mn and Fe oxides onto mesoporous SiO_2 with Mn/Fe mass ratio of 1 and calcination temperature at 400 °C, and 99.1% NO conversion rate was achieved at 160 °C, and H_2O has little effect on the catalytic activity. Guo et al. [19] prepared $\text{Ce-MnOx}/\text{Al}_2\text{O}_3$ catalysts using impregnation method. The denitration performance of the catalysts in the range of 70~300 °C was investigated. The results showed that Ce addition can improve the dispersion of MnOx on the carrier surface. 4% $\text{Ce-MnOx}/\text{Al}_2\text{O}_3$ showed good denitrification efficiency. The effect of calcination temperature on the catalytic performance was also investigated, and it found that the catalyst calcined at 550 °C contributed the best catalytic performance.

Composite manganese-based catalysts with the development of low temperature SCR catalyst, complex transition metal oxidation catalyst has been studied. Among these catalysts, the composite Mn-based catalysts were of great importance because of its wider active temperature range and higher denitration efficiency. Li et al. [14] prepared MnFeOx bimetallic oxides catalysts resulting in excellent SCR catalytic activity. The BET surface area of MnFeOx catalysts was larger than that of pure MnO_2 . The authors attributed the results to a redox reaction may occur between Mn and Fe ions

resulting in electronic transfer. The electronic transfer played a key role in the oxidation of NO to NO_2 during the NH_3 -SCR reaction of removing NOx. Zuo et al. [20] prepared Mn-Zr catalyst and found that MnOx was better dispersed when Mn/Zr molar ratio was 0.5, and the catalytic activity was strengthened due to the synergistic effect between Mn^{n+} and Zr^{4+} . Liu et al. [21] added WO_3 to the Mn-Zr catalyst. The highly dispersed WO_3 not only increased the acid sites on the catalyst surface, but also inhibited the adsorption of inert nitrates onto the catalyst surface. Wan et al. [22] synthesized NiMnOx catalysts with different molar ratios by co-precipitation. The catalyst showed highest denitration activity when the molar ratio of Ni/Mn was 0.4. It was illustrated that the catalytic performance was promoted due to the synergistic effect between Ni and Mn.

Guo et al. [23] studied the Sb modified MnTiOx catalyst and found that the average pore size of the catalyst increased due to the presence of Sb, resulting in a corresponding increase in the surface area of the catalyst. Wu et al. [28] found that adding a transition metal to the Mn/TiO_2 catalyst can improve the dispersibility of the catalyst. Wu et al. [24] prepared a series of Ce-modified MnTi catalysts and evaluated the activity of catalysts with different Ce contents. The results indicated that the addition of Ce can improve the activity of the catalyst. When the Ce content was 0.07%, the catalyst contributed the highest catalytic activity. Through the analysis of TPR and XPS, the authors found that Ce modification increased the chemical adsorption ability of oxygen and acidic sites on the surface of the catalyst, which were beneficial to the catalytic reaction. Thirupath et al. [25] doped Ni to MnOx/TiO_2 catalyst. The results showed that Ni doping improved the denitration efficiency. The presence of Ni enhanced the stability of active Mn^{4+} in the catalyst, inhibits the formation of Mn^{3+} , and improved the H_2O and SO_2 resistance. Shen et al. [26] doped Fe in $\text{Mn-Ce}/\text{TiO}_2$, and the catalyst showed good activity when the molar ratio of Fe/Ti was 0.1. The addition of Fe also improved the resistance ability of H_2O and SO_2 for the catalyst, and resistance ability was strengthened with the increase of Fe content until Fe content was 0.15%. Huang et al. [27] studied in detail the modification effect of Fe on Mn/mesoporous silica catalysts. It was found that the addition of Fe greatly improved the denitration performance of the catalyst, especially when the molar ratio of Fe to Mn was 1:1. The conversion of NO increased by about 40% at 100 °C; the characterization results show that the addition of Fe mainly improves the thermal stability and dispersion of Mn. Qiu et al. [29] studied the denitration performance of $\text{Co-Ce-Mn}/\text{TiO}_2$ catalysts formed by the addition of Co and Ce. It was found that the addition of Co and Ce increased the redox and the acidity of the catalyst compared with the Mn/TiO_2 catalyst. The addition of Co will produce a large amount of B acid sites, which is beneficial to the adsorption of NH_3 , and the addition of Ce is beneficial to the formation of NH_4^+ . Qi et al. [30] investigated the effects of the addition of different elements (Fe, Cu, Zr and Pr) on the activity of MnOx-CeO_2 catalyst and N_2 selectivity. The results showed that the addition of Fe and Zr could significantly increase the denitration activity of the catalyst in the range of 100-180 °C, but the N_2 selectivity did not change. The addition of Pr

was opposite, which could increase the selectivity of N_2 and reduce denitration activity. Cu has no significant effect on denitration activity and N_2 selectivity. These changes are determined by the reduction performance and chemisorption capacity of the catalyst.

Changing catalyst preparation methods Tang et al. [31] synthesized MnO_2 catalysts with different methods. It was found that MnO_2 prepared by solid phase method and rheological method exhibited excellent low temperature activity, and the conversion rate of NO_x was close to 100% at 100 °C. At the same time, the analysis showed that the amorphous state of the catalyst was the key factor for the low temperature catalytic activity. Jiang et al. [32] investigated the effects of MnO_2/TiO_2 preparation methods (sol-gel method, impregnation method, co-precipitation method) on its denitration performance, and found that the catalyst prepared by sol-gel method showed the best performance, active and anti- SO_2 properties. In addition, the crystal form, specific surface area, and calcination temperature of MnO_x are also important factors affecting the low temperature denitration performance [33]. Zhang et al. [34] prepared MnO_x/TiO_2 catalysts using conventional impregnation method, ultrasonic impregnation method and sol-gel method, and employed them in SCR reactions. The results revealed that the catalyst obtained by ultrasonic impregnation gave the best catalytic activity at low temperature. The conversion rate of NO was more than 90% at 120 °C. The other two catalysts gave comparable denitration efficiency almost at 150 °C. The results illustrated that the sample using ultrasonic impregnation method exhibited higher dispersibility for active species, and more Lewis acid sites, which improved the catalytic performance. France et al. [35] synthesized Ce-Fe/ MnO_x catalyst by citric acid method. The denitration rate of Ce_{12.5}-Fe/ MnO_x was over 97% at 105~135 °C, and denitration rate decreased only 4% after passing into SO_2 . Shi et al. [33] synthesized TiO_2 with multi-stage pore structure (macroporous-mesoporous) and studied the effect of pore structure on the denitration performance of the catalyst. Compared with the non-multi-stage pore Mn/ TiO_2 catalyst, multi-stage pore Mn/ TiO_2 exhibits high low temperature denitration activity and strong sulfur resistance. The authors attributed it to the larger specific surface area and the dispersion degree of the active component Mn. In our previous work, FeMnTiO_x mixed oxides catalyst, which was synthesized with CTAB-assisted and calcined at 500 °C, showed excellent low-temperature performance in NH_3 -SCR reaction [36].

In summary, relevant research on low temperature denitration catalysts has made some progress. Compared with other types of low-temperature denitration catalysts, manganese-based catalysts have high denitration efficiency and low cost, which can basically meet the denitration needs of coal-fired power plants. However, at present, there are still many problems in low temperature denitration catalysts. For example, there are a certain amount of SO_2 and water vapor in various types of flue gas. Manganese-based catalysts exhibit poor denitration activity when H_2O and SO_2 coexist. Furthermore, the related mechanism of low temperature denitration catalyst needs to be gradually elucidated, and the working temperature window of the catalyst needs to be widened.

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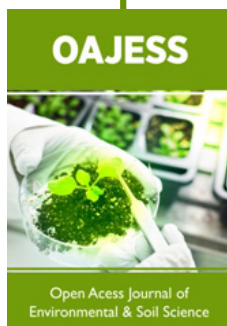


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